

Boiling and condensation heat transfer and two-phase flow of R-134a in circular microchannels

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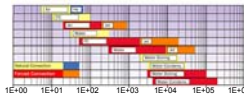
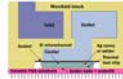
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Objectives

- Study experimentally the fundamentals of boiling and condensation heat transfer in circular microchannels.
- Investigate the conditions leading to Critical Heat Flux (CHF).
- Investigate heat transfer coefficients and pressure drops for boiling and condensation of R-134a in circular microchannels.

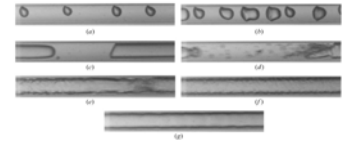
Applications: Compact micro heat sinks for electronic cooling [1]



Order of magnitude of heat transfer coefficients depending on cooling technologies.
Unit of heat transfer coefficient: W/m²-K

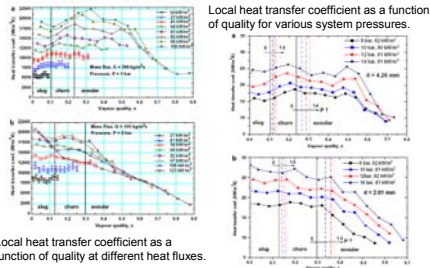


Two-phase boiling flow patterns in circular microchannels [2]



Flow observations for R-134a, $D = 0.5 \text{ mm}$, $L = 70.70 \text{ mm}$, $G = 500 \text{ kg m}^{-2} \text{ s}^{-1}$, $T_{\text{sat}} = 30 \text{ }^\circ\text{C}$ and $T_{\text{sub}} = 3 \text{ }^\circ\text{C}$, at exit of heater taken with a high definition digital video camera. (a) Bubbly flow at $x = 2\%$; (b) bubbly/slug flow at $x = 4\%$; (c) slug flow at $x = 11\%$; (d) slug/semi-annular flow at $x = 19\%$; (e) semi-annular flow at $x = 40\%$; (f) wavy annular flow at $x = 82\%$; (g) smooth annular flow at $x = 82\%$.

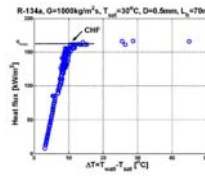
Boiling heat transfer coefficient [3]



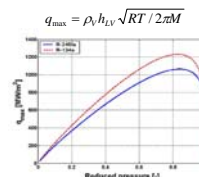
Local heat transfer coefficient as a function of quality for various system pressures.

Local heat transfer coefficient as a function of quality at different heat fluxes.

Critical heat flux [4]

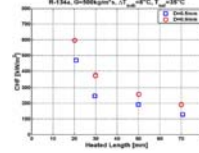


Identifying CHF



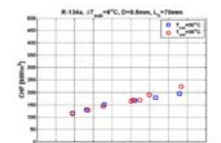
Upper limit of CHF: Theoretical prediction of CHF based on the work of Gambill and Lienhard [1].

Critical heat flux trends [4]



Variation of CHF as a function of the heated length in 0.5 and 0.8 mm ID tubes.

Influence of the refrigerant saturation temperature on CHF.



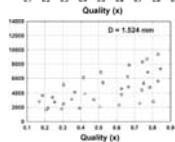
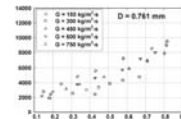
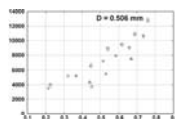
Two-phase condensation flow patterns in circular microchannels [5]

Working fluid: R-134a

Flow Regime	Flow Regimes			
	Annular	Wavy	Intermittent	Dispersed
100% Film	Discrete Wave (D)	Slug Flow	Bubbly Flow	
Annular Ring	Discrete Wave (T)	Slug Flow	Bubbly Flow	
Wave Packet	Discrete Wave (D)	Plug Flow	Bubbly Flow	
Wave Packet	Discrete Wave (D)	Plug Flow	Bubbly Flow	
Annular Film				

Note: Numbers above denote intensity of secondary waves.

Condensation heat transfer coefficient [6]



Working fluid: R-134a

Heat transfer coefficient increases with increasing mass flux and quality, and decreasing channel diameter.

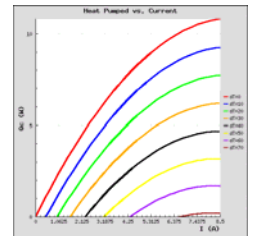
Thermoelectric coolers (TECs) [7]



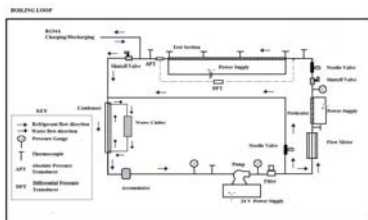
• Thermoelectric Coolers (also known as Peltier coolers): An applied voltage and current causes a temperature difference between the two faces of the cooler, thus cooling one side and heating the other.

• TECs will replace fluid to fluid heat exchangers in the condensation loop

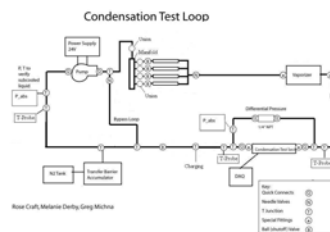
• Through calibration curves (shown on the right), the heat removed from the test section can be known by electrical measurements, thus giving more accuracy than fluid to fluid heat exchangers



Boiling loop schematic



Condensation loop schematic



Acknowledgements

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References

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